PATENT COOPERATION TREATY

PCT

INTERNATIONAL PRELIMINARY REPORT ON PATENTABILITY

(Chapter II of the Patent Cooperation Treaty)

(PCT Article 36 and Rule 70)

REC'D 3 1 OCT 2005

Applicant's or agent's file reference		WIPO PCT
P10970PC	FOR FURTHER ACTION	See Form PCT/IPEA/416
International application No. PCT/DK2004/000462	International filing date (day/month/year) 28.06.2004	Priority date (day/month/year) 27.06.2003
International Patent Classification (IPC) or a CO2F11/04	national classification and IPC	27.00.2003
Applicant BIO ENERGI APS I		
This report is the international pre- Authority under Article 35 and trail This REPORT consists of	eliminary examination report, established be nsmitted to the applicant according to Artic	py this International Preliminary Examining
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The report is also accompanied b	V ANNEXES comprise	
Sheets of the deserving	o the International Bureau) a total of 5 sh	eets, as follows:
and/or sheets containing Administrative Instruct	ng rectifications authorized by this Authoritions).	en amended and are the basis of this repo
beyond the disclosure Supplemental Box.	de earlier sheets, but which this Authority of in the international application as filed, as	considers contain an amendment that goes
Seguence listing and the seguence	<i>ureau only)</i> a total of (indicate type and nu les related thereto, in computer readable f Listing (see Section 802 of the Administrat	make a set of the second
. This report contains indications rela	ating to the following items:	
Box No. I Basis of the opin		
☐ Box No. II Priority	ioti	•
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Box No. IV Lack of unity of in	nt of opinion with regard to novelty, inventi	ive step and industrial "
M		otop and industrial applicability
⊠ Box No. V Reasoned statem applicability; citation	nontundas Aut t. ann.	
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INTERNATIONAL PRELIMINARY REPORT ON PATENTABILITY

International application No. PCT/DK2004/000462

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-	Box No. I Basis of the repo	
 With regard to the lánguage, this report is based on the international application filed, unless otherwise indicated under this item. 		nis report is based on the international application in the language in which it was
	J J =	nslations from the original language into the following language , translation furnished for the purposes of:
	☐ international search (un☐ publication of the intern☐ international preliminary	der Rules 12.3 and 23.1(b)) ational application (under Rule 12.4) v examination (under Rules 55.2 and/or 55.3)
2. With regard to the elements* of the international and it		f the international application, this report is based on (replacement sheets which
	Description, Pages	
	1-11	as originally filed
	Claims, Numbers	·
	1-42	filed with telefax on 17.10.2005
Drawings, Sheets		
	1/4-4/4	as originally filed
	☐ a sequence listing and/or ar	ny related table(s) - see Supplemental Box Relating to Sequence Listing
3.	☐ The amendments have resu	ulted in the cancellation of:
	☐ the description, pages☐ the claims, Nos.	
	☐ the drawings, sheets/figs	
	☐ the sequence listing (specific any table(s) related to se	ecify): equence listing (specify):
4.	This report has been established as if (some of) the amendments annexed to this report and listed below had not been made, since they have been considered to go beyond the disclosure as filed, as indicated in the Supplemental Box (Rule 70.2(c)).	
•	☐ the description, pages☐ the claims, Nos.	
	the drawings, sheets/figs	
	☐ the sequence listing <i>(spe</i> ☐ any table(s) related to se	cify): Quence listing <i>(specify)</i> :
		me or all of these sheets may be marked "superseded."
		of these sheets may be marked "superseded."

INTERNATIONAL PRELIMINARY REPORT ON PATENTABILITY

International application No. PCT/DK2004/000462

Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement

1. Statement

Novelty (N)

Yes: Claims

No: Claims

1,22

Inventive step (IS)

Yes: Claims

No: Claims

2-21, 23-42

Industrial applicability (IA)

Yes: Claims

1-42

No: Claims

2. Citations and explanations (Rule 70.7):

see separate sheet

Box No. VII Certain defects in the international application

The following defects in the form or contents of the international application have been noted:

see separate sheet

Box No. VIII Certain observations on the international application

The following observations on the clarity of the claims, description, and drawings or on the question whether the claims are fully supported by the description, are made:

see separate sheet

Re Item V

Reasoned statement with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement

- The amendments filed with the telefax dated 17.10.2005 introduce subject-matter which extends beyond the content of the application as filed, contrary to Article 34(2)(b) PCT. The amendments concerned are the following: The term "containers" and the expression "with containers for holding organic waste, the containers consisting of" found in claim 1 does not appear in the application as filed. The introduction of this terms broadens the scope of the claim because in the description the only devices disclosed for holding organic waste
 - are the anaerobic tanks or reactors.

 The expression "consisting of" found in claim 22 does not appear in the application as file. This expression introduces unclarity because according to the figures and the embodiments of the description more steps are present in the process than those mentioned in claim 22.
 - Therefore this report is established as if those amendments have not been made since they go beyond the disclosure in the international application as filed (Rule 70.2(c)).
- 2. Reference is made to the following documents:
 - D1: WO 88/04282 A (WASTE ENERGY CORP) 16 June 1988 (1988-06-16)
 - D2: EP-A-0 566 056 (RECYCLING ENERGIE ABFALL) 20 October 1993 (1993-10-20)
 - D3: WO 03/097560 A (PRESECO OY ; JAERVENTIE JUSSI (FI)) 27 November 2003 (2003-11-27)
 - D4: US-A-5 431 819 (HACK PETRUS J F M ET AL) 11 July 1995 (1995-07-11)
- 3. The present application does not meet the criteria of Article 33(1) PCT, because the subject-matter of claims 1 and 22, as far as it can be understood, is not new in the sense of Article 33(2) PCT.
- 3.1 Independent claim 1 refers to an entity (biogas producing facility) comprising two or three reactors or tanks which are suitable for carrying out anaerobic reactions. The output of the first reactor is connected (not necessarily a direct connection is needed, according to the description) to the input of another reactor named

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"anaerobic tank" in the application. The output of this reactor can be connected to the first reactor or to a different reactor named "second reactor" in the application.

Document D2 discloses an installation (see Figure 1) comprising an anaerobic tank (3) in which biogas is produced, connected to (L22) an anaerobic tank (2) in which anaerobic hydrolysis is carried out, the latter (2) being connected (21) to the former (3).

The subject-matter of claim 1 is therefore not new with respect to D2.

- 3.2 Documents D1, D3 and D4 also discloses an anaerobic reactor to produce biogas, connected to an anaerobic tank in which a hydrolysis may take place and the further anaerobic digestion of the hydrolysed material in an anaerobic reactor. Therefore the subject-matter of claim 1, is not new with respect to D1, D3 or D4.
- 3.3 Document D3 discloses a method of producing biogas (see figure 2, 6, reference sign 90) comprising the steps of: digestion in a reactor (88), subsequent hydrolysis (62) and feeding the hydrolysed material (66) to the first reactor. Therefore the subject-matter of claim 22 is not novel with respect to D3.
- 3.4 Documents D1, D2 and D4 appear also to disclose an anaerobic step to produce biogas, connected to an anaerobic tank in which a hydrolysis may take place and the further anaerobic digestion of the hydrolysed material. Therefore the subject-matter of claim 22 is not new with respect to D1, D2 or D4.
- 4. Dependent claims do not appear to contain any additional features which, in combination with the features of any claim to which they refer, meet the requirements of the PCT with respect to novelty and inventive step because those features have already been described in the cited documents or can presently only be regarded as merely defining options, possibilities or normal design procedures and thus would not comply with Article 33(1)(3) PCT in respect of novelty and/or inventive step.

Re Item VII

 The features of the claims should be provided with reference signs placed in parentheses (Rule 6.2(b) PCT).

INTERNATIONAL PRELIMINARY REPORT ON PATENTABILITY (SEPARATE SHEET)

International application No.

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- According to the requirements of Rule 11.13(m) PCT the same feature shall be denoted by the same reference sign throughout the application. This requirement is not met in view of the use of 12 in Figure 4 to designate the hydrolysis tank and 6 in Figures 1-3 to designate the same feature.
- 3. To comply with the requirements of Rule 5.1(a)(ii)PCT, the relevant background art disclosed in the documents D1, D2, D3 and D4 should have been mentioned in the description.

Re Item VIII

Dependent claim 2 and claims 3 to 21 when depending on claim 2 relate to a method or use, not an apparatus (Art. 6 PCT in combination with Rule 6.3(a)). Such claims should be drafted in terms of apparatus features.

CLAIMS

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- A biogas producing facility with containers for holding organic waste, the containers consisting of
- a first reactor for holding organic waste for production of biogas by digestion and having an output for digested waste and an output for produced biogas, and an anaerobic tank with an input that is connected to the first reactor output for digested waste for anaerobic hydrolysis of the digested waste and having an output for hydrolysed material that is connected to an input selected from the group consisting of an input of the first reactor and an input of a second reactor for adding hydrolysed material to the content of the respective reactor.
 - A biogas producing facility according to claim 1, wherein the anaerobic hydrolysis is performed at a pressure that is substantially equal to the saturation vapour pressure during a period of the anaerobic hydrolysis.
- A facility according to claim 1 or 2, wherein the output for hydrolysed material is
 connected to an input of the first reactor.
 - A facility according to claim 1 or 2, wherein the output for hydrolysed material is connected to an input of the second reactor.
 - 5. A facility according to any of the preceding claims, further comprising a separator with an input that is connected to the first reactor output for digested waste for selective separation of particles larger than a predetermined threshold size from the digested waste and an output for the separated large particles that is connected to the input of the anaerobic tank.
 - 6. A facility according to claim 5, wherein the separation efficiency is enhanced by adding precipitation agents or polymers upstream the separator whereby the particle size upstream the separator is increased leading to improved retention of solids for downstream hydrolysis.
 - A facility according to claim 5 or 6, wherein the threshold size is larger than or equal
 to a value selected from the group consisting of 0.1 cm, 0.2 cm, 0.5 cm, 1.0 cm, 1.5
 cm, and 2.0 cm.
- 30 8. A facility according to any of claims 5-7, wherein the separator further comprises a dewatering device for dewatering of the separated particles.

- A facility according to any of the previous claims, wherein the anaerobic tank further comprises an input for reception of organic waste material in the tank for anaerobic hydrolysis together with digested material from the first reactor.
- 10. A facility according to any of the previous claims, wherein the hydrolysis is performed at a temperature range and for a time range selected from the group consisting of 50 °C 75 °C for 0,25 to 24 hours, 70 °C 100 °C for 0,25 to 16 hours, 100 °C 125 °C for 0.25 to 8 hours, 125 °C 150 °C for 0.25 to 6 hours, 150 °C 175 °C for 0.25 to 4 hours, and 175 °C 200 °C for 0.25 to 2 hours.
- 11. A facility according to any of the preceding claims, wherein the anaerobic tank is further connected to a pressure source for provision of a pressure in the anaerobic tank above 1 atmosphere.
 - 12. A facility according to any of the preceding claims, further comprising a partitioning device for partitioning of organic waste and having an output for supplying the partitioned waste to the first reactor.
- 13. A facility according to any of the preceding claims, further comprising a tank for mixing a waste material with high dry matter content mixed with livestock dung and feeding the mixture into the first reactor.
 - A facility according to claim 13, wherein the waste material with high dry matter content comprises straw.
- 20 15. A facility according to any of the preceding claims, further comprising a tank for mixing a waste material with high dry matter content with hydrolysed material from the anaerobic tank and feeding the mixture to the first reactor.
 - A facility according to claim 15, wherein the waste material with high dry matter content comprises straw.
- 25 17. A facility according to any of claims 1-14, further comprising a tank for mixing a waste material with high dry matter content with hydrolysed material from the anaerobic tank and feeding the mixture to the second reactor.
- 18. A facility according to claim 17, further comprising a second separator that is connected to the second reactor output for selective separation of particles larger than a predetermined threshold size from the digested waste and having an output for the separated large particles, and wherein the anaerobic tank is connected to the second separator output for hydrolysis of the separated particles.

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- 19. A facility according to claim 18, wherein the second separator further comprises a second dewatering device for dewatering of the separated particles.
- 20. A facility according to any of claims 17-19, wherein the waste material comprises straw.
- 21. A facility according to any of the preceding claims, wherein the anaerobic tank has a gas output for supplying gas produced during hydrolysis to be combined with biogas output from the first reactor.
 - A method of producing biogas consisting of the steps of producing biogas by digestion of organic waste in a reactor,
- subsequently performing an anaerobic hydrolysis of digested waste in an anaerobic hydrolysis tank, and

 feeding the hydrolysed material to an input selected from the group consisting of an input of the first reactor and an input of a second reactor for adding hydrolysed material to the content of the respective reactor for further digestion and gas
 - 23. A method according to claim 24, wherein the anaerobic hydrolysis is performed at a pressure that is substantially equal to the saturation vapour pressure during a period of the anaerobic hydrolysis.
- 24. A method according to claim 24 or 25, wherein the output for hydrolysed material is fed into the first reactor.
 - 25. A method according to claim 24 or 25, wherein the output for hydrolysed material is fed into the second reactor.
 - 26. A method according to claim 22, wherein the step of producing biogas further includes selective separation of particles larger than a predetermined threshold size from the digested waste and feeding the separated particles into the hydrolysis tank.
 - 27. A method according to claim 28, wherein the separation efficiency is enhanced by adding precipitation agents or polymers upstream the separator whereby the particle size upstream the separator is increased leading to improved retention of solids for downstream hydrolysis.
- 30 28. A method according to claim 28 or 29, wherein the threshold size is larger than or equal to a value selected from the group consisting of 0.1 cm, 0.2 cm, 0.5 cm, 1.0 cm, 1.5 cm, and 2.0 cm.

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- 29. A method according to any of claims 28-30, wherein the separation includes dewatering of the separated particles.
- 30. A method according to any of claims 24-31, wherein the step of anaerobic hydrolysis includes inputting organic waste material into the tank for anaerobic hydrolysis together with digested material from the first reactor.
- 31. A method according to any of claims 24-32, wherein the hydrolysis is performed at a temperature range and for a time range selected from the group consisting of 50 °C 75 °C for 0,25 to 24 hours, 70 °C 100 °C for 0,25 to 16 hours, 100 °C 125 °C for 0.25 to 8 hours, 125 °C 150 °C for 0.25 to 6 hours, 150 °C 175 °C for 0.25 to 4 hours, and 175 °C 200 °C for 0.25 to 2 hours.
- 32. A method according to any of claims 24-33, wherein the anaerobic hydrolysis is performed at a pressure above 1 atmosphere.
- 33. A method according to any of claims 24-34, wherein the step of producing biogas by digestion of organic waste includes partitioning organic waste and supplying the partitioned waste to the first reactor.
- 34. A method according to any of claims 24-35, wherein the step of producing biogas by digestion of organic waste includes mixing waste material with high dry matter content mixed with livestock dung and feeding the mixture into the first reactor.
- 35. A method according to claim 36, wherein the waste material with high dry matter
 content comprises straw.
 - 36. A method according to any of claims 24-37, wherein the step of producing biogas by digestion of organic waste includes mixing a waste material with high dry matter content with hydrolysed material from the anaerobic tank and feeding the mixture to the first reactor.
- 25 37. A method according to claim 38, wherein the waste material with high dry matter content comprises straw.
 - 38. A method according to any of claims 24-37, wherein the step of feeding the hydrolysed material includes mixing a waste material with high dry matter content with hydrolysed material from the anaerobic tank and feeding the mixture to the second reactor.
 - 39. A method according to claim 40, wherein the step of performing anaerobic hydrolysis includes selective separation of particles larger than a predetermined threshold size

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from the digested waste in the second reactor and feeding the separated particles into the hydrolysis tank.

- 40. A method according to claim 41, wherein the separation includes dewatering of the separated particles.
- 5 41. A method according to any of claims 40-42, wherein the waste material comprises straw.
 - 42. A method according to any of claims 24-43, wherein the step of hydrolysis includes combining gas produced during hydrolysis with biogas output from the first reactor.